

# Hydrogen and fuel cell stationary applications: key findings of modelling and experimental work in the HYPER project



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# Outline



- Introduction to HYPER
- Who is involved?
- Phenomena considered for modelling and experimental work
- How is the work grouped? Scenarios considered?
- Snapshot of key activities and results in each scenario – detailed descriptions in other ICHS 3 papers
- Main conclusions

# Introduction to HYPER



- Installation **Per**mitting Guidance (IPG) for Small Stationary **Hy**drogen and Fuel Cell Systems
- EC FP6 specific targeted research project
- HYPER: Develop guidelines to enable fast track approval of safety and procedural issues
- Aimed at developers, design engineers, manufacturers, installers and authorities
- November 2006 –January 2009
- Extensive modelling and experimental programme to:
  - **Generate new scientific knowledge and data**
  - **Where possible use this data as a basis for IPG**



# Who was involved?

- Collaboration between 15 partners from the European community, Russia and USA
- 9 Partners contributed to work presented here



# Programme of work



- Gap analysis performed
- Relevant topics identified:
  - High pressure release / low pressure release
  - Moderate – foreseeable release / catastrophic release
  - Explosive atmosphere: inside equipment casing / outside equipment casing
  - Explosive atmosphere inside room/building
  - Quiescent / turbulent explosive atmosphere, Early ignition / late ignition
  - Explosion / jet fire; Mitigated / non mitigated scenarios
- Key scenarios for further modelling and experimental work
  1. High pressure releases: typical of those associated with storage
  2. Small foreseeable releases; around the FC etc
  3. Catastrophic releases: combustion inside the FC
  4. The effect of walls and barriers
  5. Sensors and detection



# High Pressure Releases

# Overview and objectives

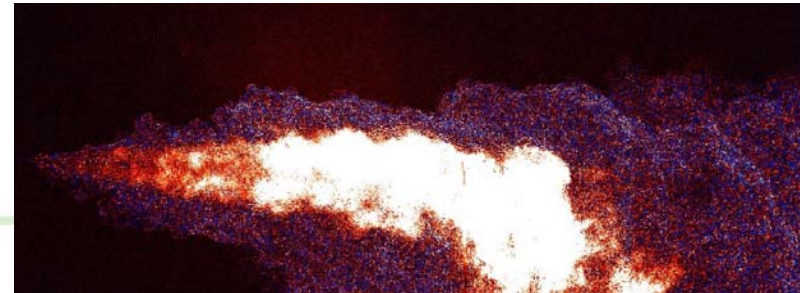


- Relates to failure of **high pressure hydrogen storage**
- Pressures in experiments up to 900+ bar (INERIS) , pipe diameters up to 10 mm (HSL)
- Data from the literature used to support modelling (UU, CEA)
- Assess the hazard on failure of pipe-work/components and how the risk of this hazard causing injury or further damage can be minimised.
- Phenomena studied:
  - **jet fires, unignited jets,**
  - **delayed ignition of a flammable cloud formed by a release**
- Better understanding and evaluation of the risks
- Enables estimation of safety distances

# HSL experiments



- Release scenarios included effect of **jet attachment** and of varying: **orifice size, ignition delay and ignition position**
- Flammability envelope, flame size and heat fluxes for various geometries and pressures investigated
- Restrictors 1.5, 3.2 and 6.4 mm, full bore 9.5mm
- Change ignition timing and location
- 205 bar to free air
- Flame lengths are longer in the case of attached jets
- Max overpressure versus ignition position given among other results
- **See ICHS 3 Paper for further details**



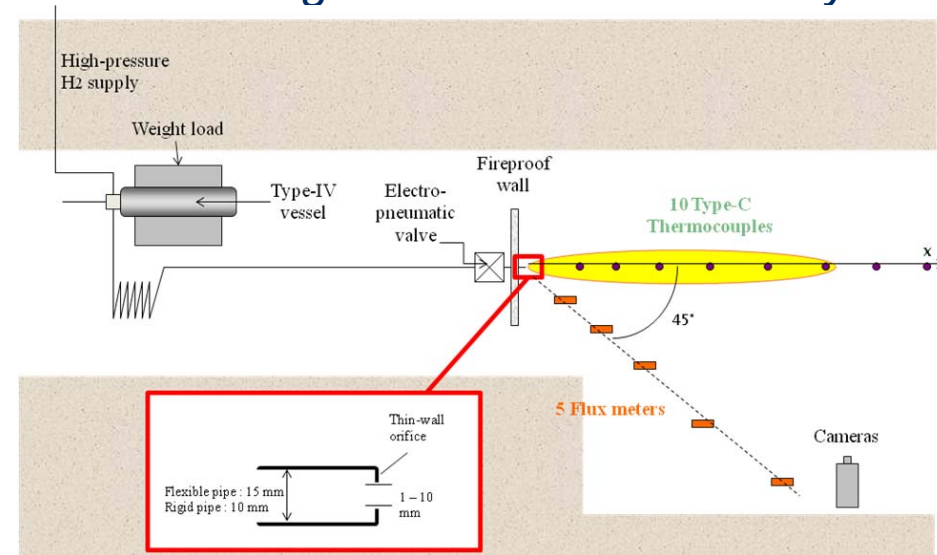


# INERIS INERIS experiments



- 80m long gallery, 12m<sup>2</sup> cross section
- Jet fires
- Low pressure tests (100 bar)
- High pressure tests (900 bar)
- Orifices: 1, 2, 3, 4, 7 and 10 mm
- Horizontal jet, 1.5m above ground level
- Flame length results shown later on nomogram
- Max width: length  $\approx$  1/6

Figure: Schematic of facility



- See ICHS 3 Paper for further details

## CEA:

- Dispersion cloud in large domain
- Subsequent combustion
- Takeno experiments of delayed ignition  
*[Takeno K. et al. Phenomena of dispersion and explosion of high pressurized hydrogen, 2nd ICHE, 2007 San Sebastian, Spain]*
- 10mm piping, 400 bar, horizontal release
- Reactive, fully compressible (Cast3m)

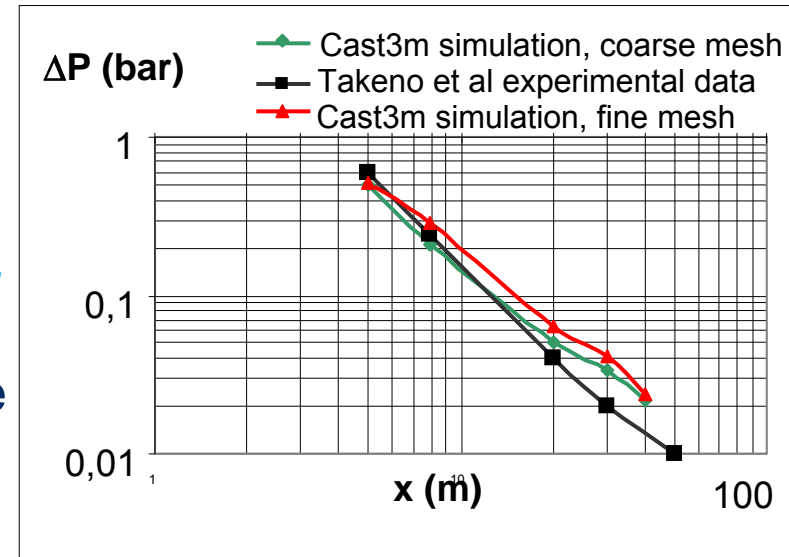
## UU:

- **Parametric study of free jet fires**

UU equivalent diameter method, LES, validated approach

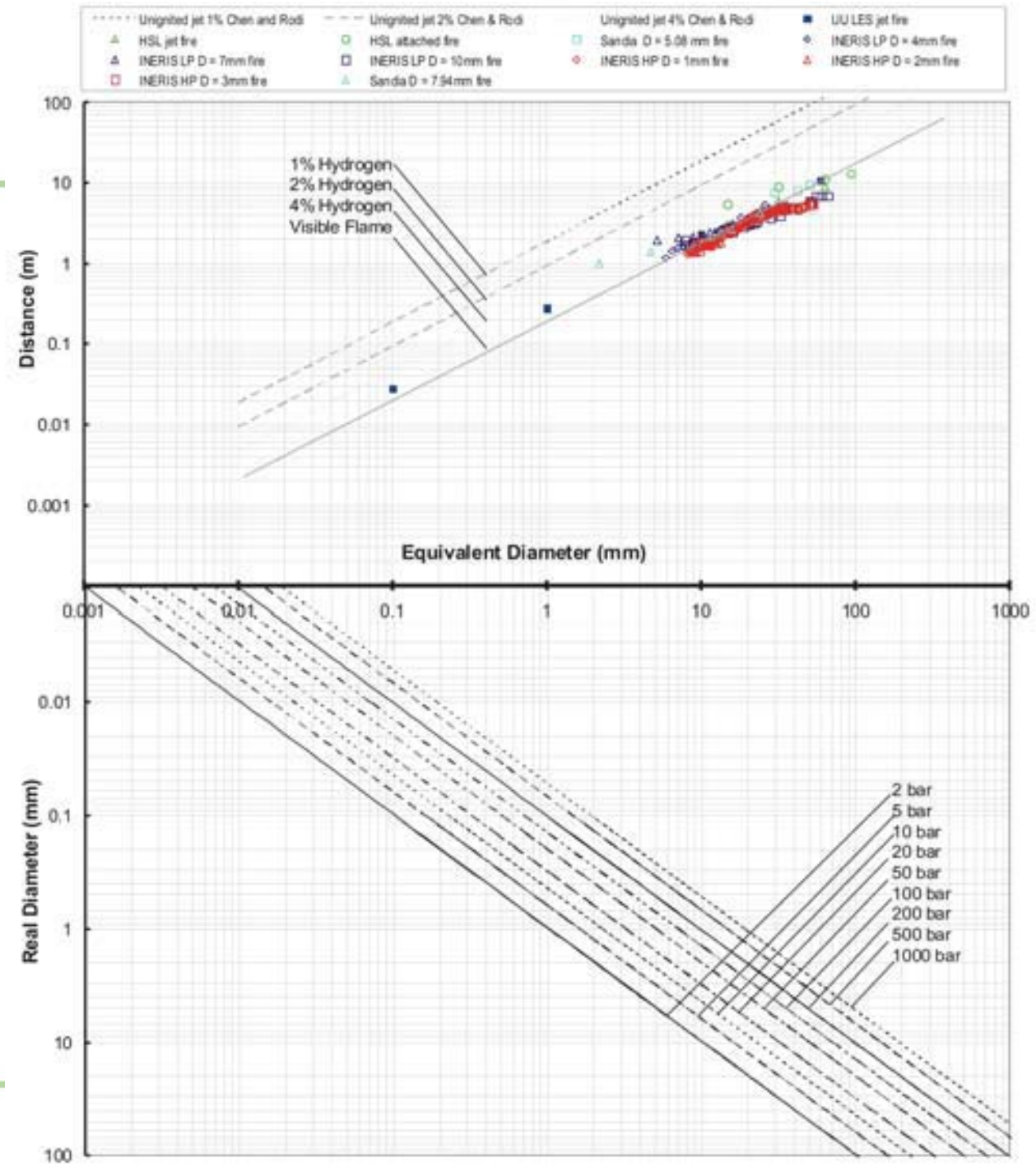
Equivalent diameters 0.1mm to 100mm

Maximum overpressure



**Engineering  
Nomogram**  
incl. simulations,  
INERIS and HSL  
data

Further  
developments  
since HYPER





# Small Foreseeable Releases

# Overview and objectives



- Concerns “small” leaks that could potentially be controlled through ventilation
- Related to low-pressure hydrogen downstream of the pressure regulation controlling the flow of hydrogen to the fuel cell system.  
(Leaks originating inside the fuel cell)
- Phenomena studied:
  - Dispersion of hydrogen
  - Concentration of H<sub>2</sub> for various natural and mechanical ventilation configurations
- Experimental work at UNIPI, Modelling work at NCSRD and UU

Work focused on the case of a fuel cell system located inside a typical enclosure. Ventilation configurations were varied to assess the resultant concentration of H<sub>2</sub> for different low leak rates

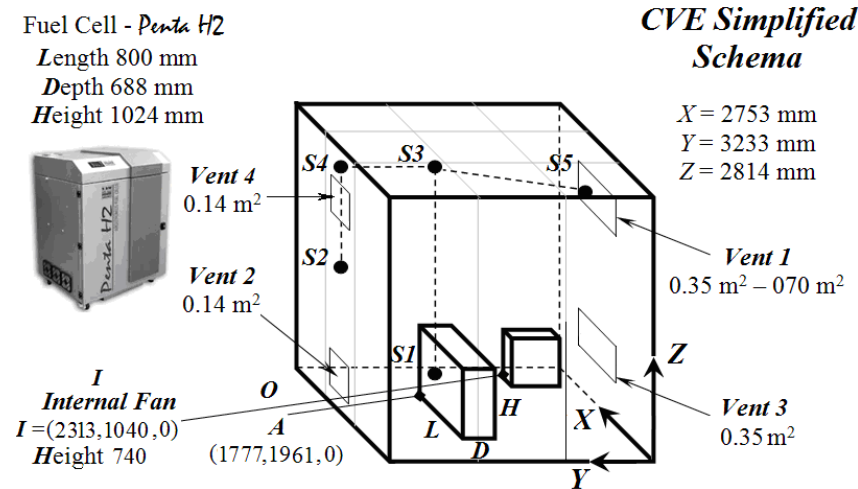


# UNIFI experiments



- Determine ventilation requirements such that concentration of  $H_2$  in air for Zone 2 ATEX (2% v/v) is not exceeded
- Volume of reference enclosure:  $25 \text{ m}^3$
- Vary leak rate, vent location and vent area  
(min  $0.35 \text{ m}^2$ , max  $2.5 \text{ m}^2$ )
- Worst case of 5 bar taken
- Leak area:  $0.25 \text{ mm}^2$  (ATEX guidance)
- Gives max flow of 40 l/min
- Areas of  $0.5 \text{ mm}^2$  and  $1 \text{ mm}^2$  also
- Natural Ventilation (NV):  
40 l/min, 90 l/min and 180 l/min
- Forced ventilation (FV):  
same rates + 2 fan flow rates
- FV tests were performed in cases where NV failed i.e. when  $H_2$  %vol was not  $\leq 2\%$

Figure: CVE Facility, showing sampling points and vent areas





## NCSR

- Majority of UNIPi's NV experiments simulated by NCSR
- ADREA-HF code
- Model included FULL interior of the FC
- See papers at ICHS 3 for full details!

## UU

- UU investigated the effect of wind on the efficiency of NV
- Wind was directed oncoming to the upper vent
- Air velocities of 0, 0.11, 0.33 and 1.1 m/s

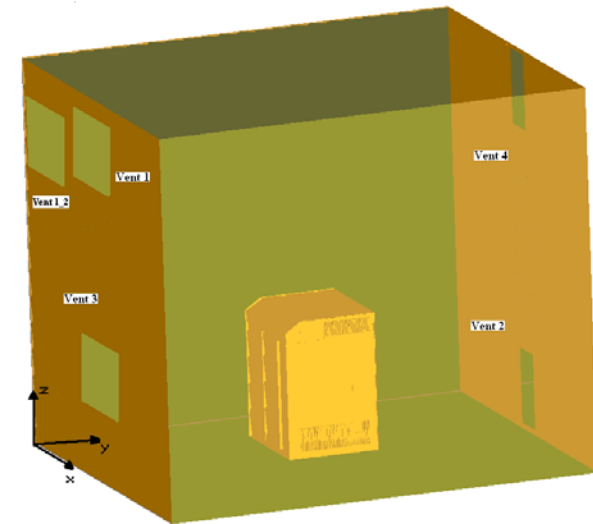
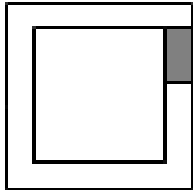
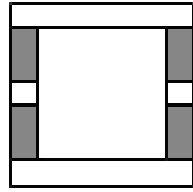


Figure : Facility and FC  
(DELTA-B Code)



# Experimental results



- Full results and table can be found in the paper
- Natural ventilation is deemed to be “effective” only if ATEX zone 2 is respected
- Natural ventilation is effective when considering the worst leak (40 l/min) from the 5 bar pipe, except in the configuration with 1 upper vent 
- For a higher leak rate of 90 l/min the natural ventilation is effective only for a configuration with 4 vents ( 2 upper and 2 lower on opposing sides of enclosure) 
- For the maximum leak rate of 180 l/min natural ventilation is ineffective
- Both forced and natural ventilation results are given in the paper





## NCSR D

- Good agreement between predicted and experimentally measured concentration time histories
- Comparison for test 3, release flow rate of 40l/min shown (nozzle diameter of 1mm and 1 vent open, horizontal release)
- See additional ICHS 3 paper

## UU

- The ambient wind was found to worsen H<sub>2</sub> venting in a very narrow range of velocities
- In a realistic scenario effect may be diminished further as a result of turbulent fluctuations in wind both in velocity value and direction

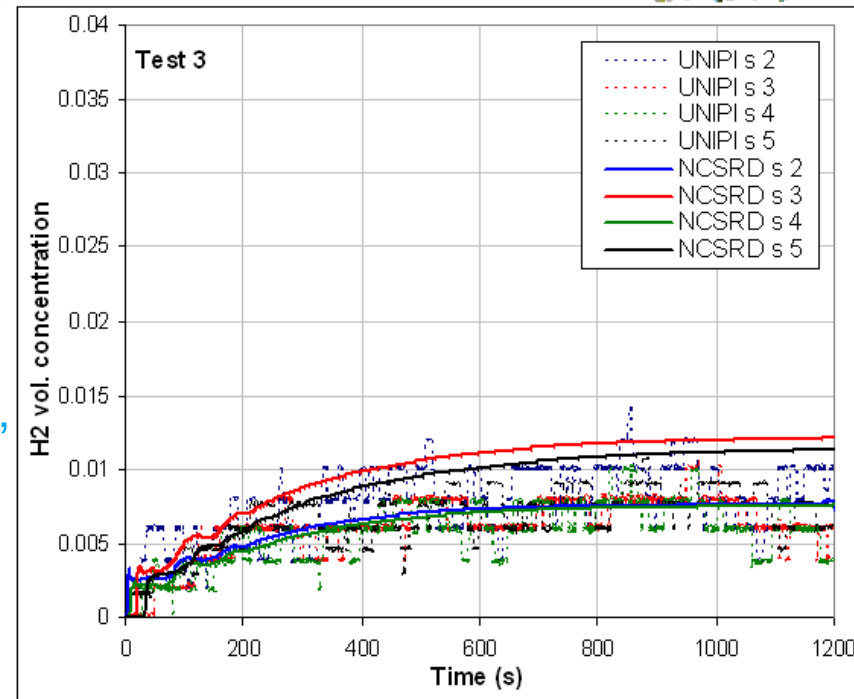


Figure : UNIPi-NCSR D comparison (sensors 2, 3, 4 and 5)





# Catastrophic Releases

# Overview and objectives



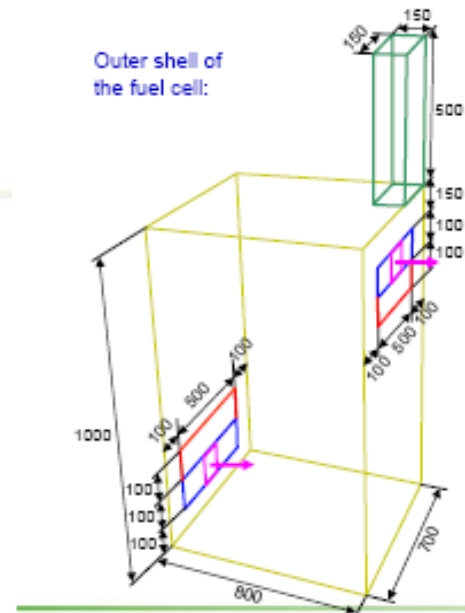
- Considers the **rupture of the hydrogen feed line inside the fuel cell**
- Hazard potential of a severe leakage investigated
- Experimental work performed by Pro-Science
- H<sub>2</sub> release rates of 1.5 g/s, up to 15g/s considered for a duration of 1s
- Phenomena studied:
  - **Dispersion of hydrogen**
  - **Subsequent ignition of the hydrogen air mixture**
- Objectives:
  - Determine if DDT occurs and order of overpressures
  - Assess effects of internal blockage ratio
- Modelling work by CEA included validation and assessment of overpressures

## Pro-Science Experiments

- Generic FC cabinet, with generic FC enclosure model
- Internal volume of 560 l, minimum blockage of 120 l
- H<sub>2</sub> release rates of 1.5 - 15g/s for a duration of 1s
- 3 cases, with 3 different venting characteristics
  - two opposing vent openings – passive (1a) and active venting (1b)
  - two enlarged opposing vents, doubled size – passive (2)
  - case with smaller vents + chimney at the top (3)
- Dispersion and combustion experiments
- 2 internal blockage ratios (50% & 67%), 2 ignition positions (inside & outside)
- 2 ignition times (immediate continuous and after 4s for 300ms)

## CEA Simulations

- Distribution & combustion, case 1a, H<sub>2</sub> release rate of 6g/s, ignition 4s
- Fluent (dispersion), Cast3m with CREBCOM combustion model (combustion)





## Dispersion experiments

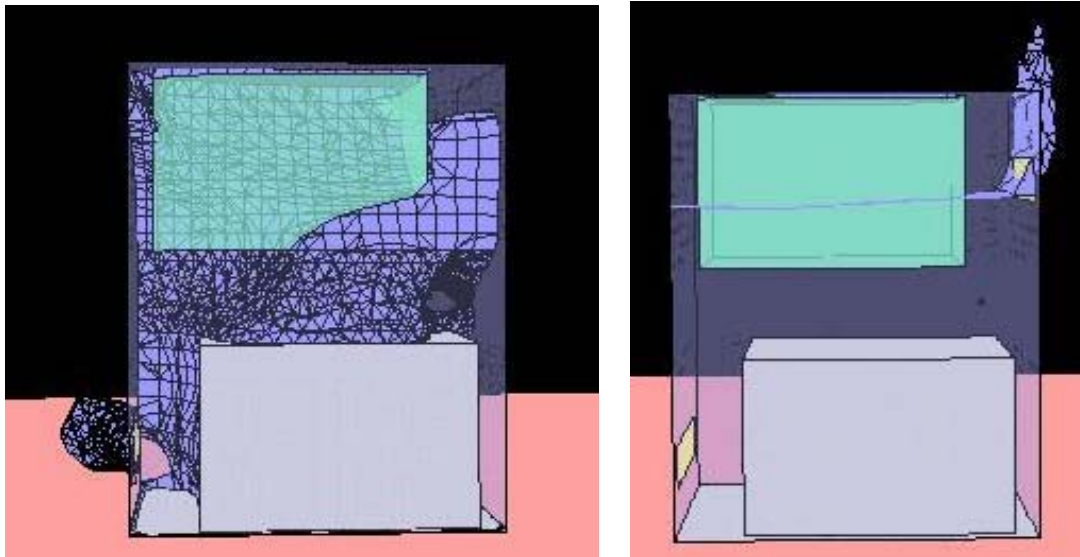
- Low internal obstruction: - “Chimney effect” in all experiments
- High internal obstruction:
  - outside enclosure: only small H<sub>2</sub> concentrations measured
  - inside: inhomogeneous mixture with high concentrations near walls and top
  - no combustion experiments with such geometry due to high concentrations

## Combustion experiments

- Combustion in all cases of durable internal ignition even 1.5g H<sub>2</sub>
- Ignition of 3g H<sub>2</sub> > pressure waves max. 40mbar (breakage of large windows)
- Ignition of 4g H<sub>2</sub> > pressure waves max 100mbar (human injury)

See Pro-Science ICHS 3 paper for full details

- Qualitatively experimental results were recovered
- At 4s, when ignition occurs, simulation predicts flammable mass of 5.5g
- Combustion simulations showed flame acceleration occurred in the cube obstacle and close to the rear wall leading to high overpressures
- For a remaining mass of H<sub>2</sub> mass in FC, predicted overpressure 0.2bar



*Figure : Isosurface 4% H<sub>2</sub> after 0.31 s (L), and 21.5 s (R)*



# The Effect of Walls and Barriers

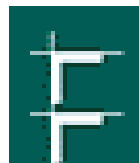


# Overview and objectives

- Concerned with the use of barriers to control the impact of releases from high pressure hydrogen storage.

## Objectives:

- Determine barrier wall effectiveness as a mitigation strategy
- Determine the resulting overpressures and radiation
- Various angles of impingement are considered
  
- Experimental and modelling work by Sandia (HSL not described here)
- Additional papers at ICHS 3 by Sandia
- Modelling work FZK



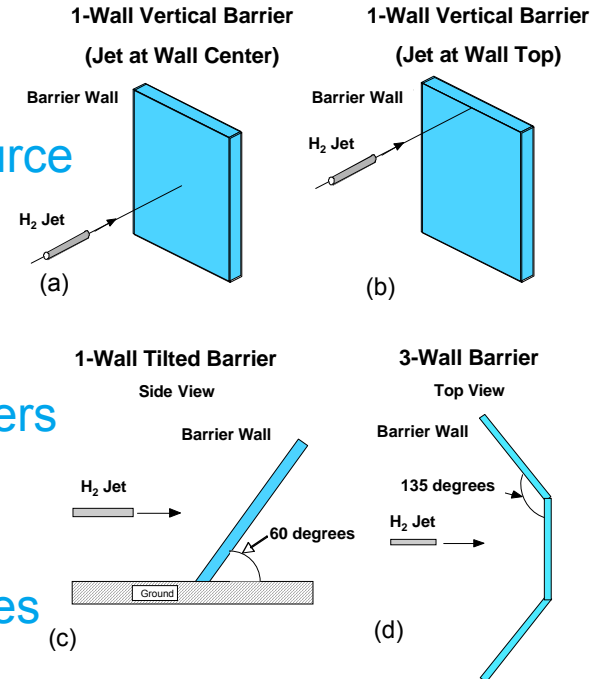
LABORATORIUM  
Forschungszentrum Karlsruhe  
in der Helmholtz-Gemeinschaft





## Sandia modelling and experimental programme

- Experimental measurements included:
  - Study of initial flame propagation from ignition source
  - Ignition overpressures, wall deflection, radiative heat flux, wall and gas temperature
- Modelling included: (FUEGO and FLACS codes)
  - 3D calculations of jet flame deflection by the barriers
  - thermal radiation field around barriers
  - predicted overpressures from ignition concentration field - deflected unignited H<sub>2</sub> releases
- 4 barrier wall tests and 1 free jet as a baseline



## FZK modelling

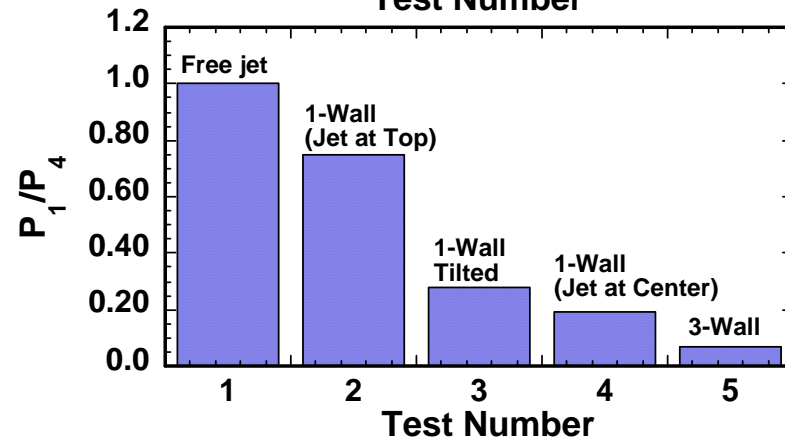
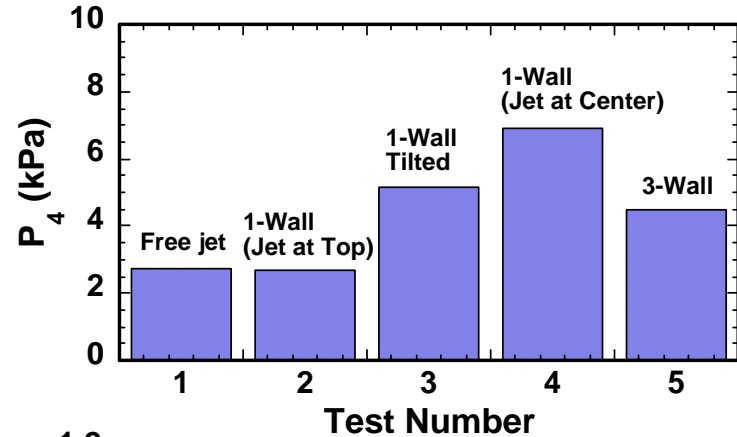
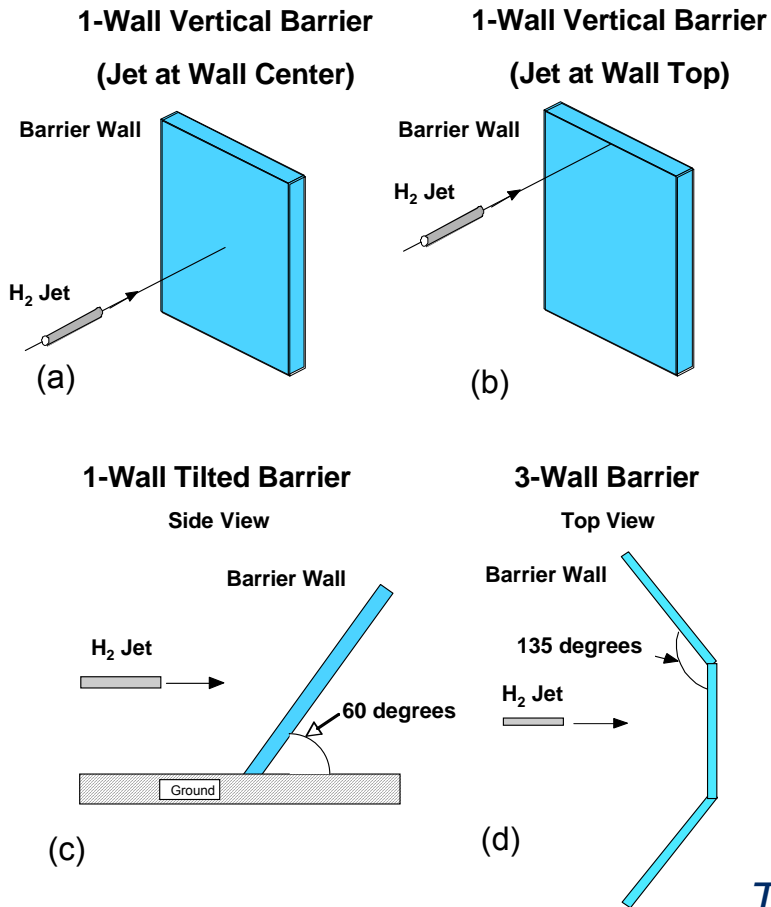
- Two geometries simulated: free jet and impingement in wall centre
- COM3D code, ignition at 140, 260 & 640ms
- Results deemed of acceptable accuracy for practical purposes



# Sandia results



See ICHS 2 and 3 papers for further details



Top graph: Max. overpressure measured prior to wall;

Lower graph: Ratio of max. overpressure measured after the wall to that prior to the wall.

# Conclusions (1/2)



## High Pressure Releases:

- Engineering nomogram can be used to estimate flame length, or extent of the flammable envelop, for a given storage pressure and diameter
- Inclusion of flow restrictors in supply lines reduces flame length
- When a jet is orientated close to a surface, jet length may be enhanced
- Ignition in weak region of the cloud: slow burn and smaller overpressure

## Small Foreseeable Releases:

- Where possible, it is recommended to use one or more suitable solutions:
- Increase vent areas beyond the min. value calculated using ATEX;
- Incline the roof making the NV easy and efficient
- Install a small fan able to remove the internal mixture from the enclosure.

# Conclusions (2/2)



## Catastrophic Releases:

- Reduce the H<sub>2</sub> amount that can be released from a ruptured pipe inside the FC enclosure to below 1.5 g.
- The feed line pressure and/or diameter should by design limit the flow rate to what is necessary for FC consumption (inventory 1g for case studied)
- The release duration should be reduced as much as possible
- Obstacles should be avoided by a careful design of the cell itself
- Vent design should allow for a rapid dispersion of H<sub>2</sub> during a leak and efficient pressure relief during an explosion

## The effect of walls and barriers:

- For the conditions investigated the barrier configurations studied:
- Reduced horizontal jet flame impingement hazard by deflecting the flame
- Reduced radiation hazard distances for horizontal jet flames
- Reduced horizontal unignited jet flammability hazard distances

**Overall the modelling and experimental work in HYPER provided insight into the key scenarios related to the safety of stationary FC systems**

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For further information the HYPER Installation Permitting Guidelines are available online

<http://epshypp.web.its.manchester.ac.uk/>

