

IGNITED RELEASES OF LIQUID HYDROGEN: SAFETY CONSIDERATIONS OF THERMAL AND OVERPRESSURE EFFECTS

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Background



- HSE funded research program
- If hydrogen economy takes off there will be an increase in LH2 road tanker traffic in UK
- Increase in refuelling operations
- Therefore a need to assess the risk from a delivery hose failure in standard operation





- Commissioned as four programs of work:
 - Positions paper: Hazards of LH2 (RR769)
 - Un-ignited releases
 - Computational modelling of the releases (un-ignited)
 - Ignited releases

Project aims



- Flammable extent of a vapour cloud
- Flame speeds through a vapour cloud
- Radiative heat levels generated during ignition







• P&ID of release system





- LH2 tanker containing 2.5 tonnes
- 1" n.b. horizontal release line
- Release pressure of 1barg
- Flow rate measured to be ≈ 60 litres per minute
- Ignition system:
 - 1kJ chemical igniters in four locations due to variability in cloud direction
 - Ignition positions close and far from release



Igniter positions





- Instrumentation:
 - Flammable extent and flame speed
 - Standard and IR video at 50fps
 - Some high speed video at 500fps
 - Radiative heat
 - Ellipsoidal radiometers, range: 110kW/m², 160° field of view
 - Meteorological measurement
 - Temperature, humidity, wind speed and direction



Radiometer positions





- 14 tests performed, of which 10 ignited
- Variables:
 - Release duration
 - Weather conditions (wind direction/speed)
 - Ignition position



• Video of test 2





• Video of test 3





• High speed video of test 7





IR stills of test 11



300ms post ignition

2000ms post ignition



• Test 6





'Snow' formation prior to ignition on long releases



 Secondary explosion appears to emanate from this location



Radiometer trace of test 6



Overpressure estimation



- During test 6 a one off secondary explosion occurred
- ≈ 260 second release
- Secondary explosion occurred ≈ 3 seconds after ignition
- Produced an 8m hemispherical fireball emanating 2.5m in line with release
- No pressure measurements at time of explosion, only standard video and radiometers

Overpressure estimation



Two methods used:

- 1. Pressure Effects
- Perspex windows in small cabin 20m away failed to break, therefore a maximum can be deduced
- This is modelled in Hazl©, however, nearest material available is Polycarbonate (stronger than Perspex)
- TNT equivalent calculated to be < 4kg
- If the H₂ were act like a condensed phase explosive (i.e. all H₂ used to generate blast wave) then this equates to < 150g H₂ yielding 18MJ



Two methods used:

- 2. Radiative Fraction
- Use radiometer data and relate to the radiative fraction
- Jet-fire phase used for estimate of radiative fraction

 $Q_r = \chi M \Delta H_c$

where Q_r - heat radiated, kW; χ - radiative fraction (between 0 and 1); M - mass rate of fuel combustion, kg/s; ΔH_c - heat of combustion of the fuel, kW/kg

- Normally radiative fraction based on significant distance from flame
- In this case the flame was elongated along the line of radiometers and close to the ground

Overpressure estimation



• Therefore a semi-cylindrical radiating heat source assumed:

$$Q_r = (1+\alpha)\frac{\pi dLq}{2}$$

where Q_r - heat radiated, kW; d - distance to radiometer, m; L - length of flame, m; q - heat flux at radiometer, kW/m²; α - reflection coefficient of concrete surface below the flame

- Reflection co-efficient taken as 0.55
- Giving radiative fraction of 0.054 for jet-fire phase
- Estimate is based on the furthest radiometer, a hemispherical heat flux and a similar radiative fraction as during jet-fire phase
- Gives 675g H2 yielding 82MJ, ≈ 18kg TNT equivalent!!
- Reported that H2 explosions of a particular energy would cause less damage at a given distance than a TNT explosion of same energy



• Levels of harm equated to thermal dose units (TDUs) $TDU = I^{\frac{4}{3}} \times t$

where TDU - thermal dose units; I - thermal radiation intensity, kW/m²; t - duration for which the radiation is experienced, secs

- Using the radiometer data from the ignited tests and historical IR burn severity data an assessment of the thermal dose from LH2 spills can be made
- Four test regimes considered: <u>Continuous events</u>
 - Steady state jet-fire during high wind speeds > 0.6 m/s
 - Steady state jet-fire during low wind speeds < 0.6m/s
 - Initial deflagration or 'burn back' of the release cloud to source
 - Secondary explosion seen after the initial deflagration

Instantaneous events





Continuous jet-fires

No harm 1.6kW/m² (grey area)



Time to 'pain' at 7.6m ≈ 44 seconds





Instantaneous deflagration and explosion
Test 6







Approximate safety distances



	Initial cloud deflagration	Secondary explosion	Jet-fire (High wind)	Jet-fire (Low wind)
Minimum separation distance from source to avoid 'pain' (m)	> 11.1	> 11.3	12.6 > 13.7	12.6 > 13.7
Exposure time (secs)	0	0	ø	œ
Note: These values consider radiative heat only, not pressure effects				

Conclusions



From experimentation, four separate regimes have been found to occur when a full bore failure of a 1" liquid (60 l/min) hydrogen tanker transfer hose is ignited:

- An initial deflagration of the cloud back to source, travelling at speeds up to 50 m/s
- A possible secondary explosion emanating from the solid deposit generated after the initial deflagration of the release cloud due to oxygen enrichment.
- A buoyancy driven jet-fire when wind conditions are minimal (wind speeds < 0.6 m/s), with flame speeds > 25 m/s
- A momentum dominated jet-fire when wind conditions are high (wind speeds > 0.6 m/s), with flame speeds > 50 m/s